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| (54) Thie: HIGH CONCENTRATED, SOLID MEPIQUA (57) Abstract | T CHIL | ORIDE AND CHLORMEQUAT CHLORID | E PRODUCTS |
| The present invention provides bygroscopic plant gr the powders and tablets. The most preferred formulati dimethylammonium salt. | on uses | gulator formulations in solid forms and ass an effective amount of an N,N-dimethyl | ociated methods of making -piperidinium and/or N,N- |
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High Concentrated, Solid Mepiquat Chloride and Chlormequat Chloride Products

5 Description

The present invention relates to methods for making flowable, highly concentrated powders and tablets of hygroscopic plant growth regulator compounds, and more specifically to processes to 10 dry mepiquat chloride and chlormequat chloride aqueous solutions to form flowable highly concentrated solid products.

Plant growth regulators affect the physiology of plant growth and influence the natural rhythm of a plant. More specifically, plant 15 growth regulators may, for example, reduce plant height, stimulate seed germination, induce flowering, promote or inhibit fog, darken leaf coloring, minimize lodging of cereals, slow grass growth on lawns, reduce boll rot and provide better boll retention in cotton.

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Plant growth regulators may be applied to plants in a variety of methods including different formulations. Of these various methods, use of liquid and dry compositions are the most common. The particular formulation desired and resulting efficacy enhan-25 cement will greatly depend upon the species to be treated, environmental conditions, the geographical area and the climatology of the area at the time of treatment.

The plant growth regulator, known trivially as mepiquat chloride, 30 is generally used to control various aspects of cotton boll growth. See, for example, Khafaga, Angew. Botanik 57, 257-265 (1983); Sawan et al., J. Agronomy & Plant Science, 154, 120-128 (1985); U.S. Patents 3,905,798 and 4,447,255, and "The Pesticide Manual", 9th Edition, The British Crop Protection Council, 35 Farnham, Surrey, Great Britain, Entry No. 7920.

The plant growth regulator, known trivially as chlormequat chloride, is generally used to reduce lodging of cereals (cf. "The Pesticide Manual", 9th Edition, The British Crop Protection Coun-40 cil, Farnham, Surrey, Great Britain, Entry No. 2420).

Mepiquat chloride and chlormequat chloride are used as plant growth regulators in agriculture. Mepiquat chloride and chlormequat chloride have high water solubilities of more than 1 kg/L at 45 20°C. The melting point of mepiquat chloride is 223°C, chlormequate chloride begins to decompose at 210°C.

Both substances are very hygroscopic, readily absorbing moisture from humid air, so much so, that the dry powders can turn to liquid when exposed to ambient humid air. During storage, the solid mepiquat chloride or chlormequat chloride is strongly caking and 5 sticking to container surfaces, even at low residual water contents of less than 0.5 wt.-%.

These properties make it extremely difficult to dry mepiquat chloride or chlormequat chloride. In conventional spray dryers, 10 the material is very difficult to dry. It must be atomized extremely finely to reduce the moisture to a suitable level and even then it retains too much water to dry practically. The product remains sticky and adheres to the walls of the dryer and the dryer ducts and cyclones, eventually plugging the ducts and cyclones. Furthermore, powder from such a process, because it is so fine, flows poorly out of the dryer, and upon storage in a drum, is rendered unflowable due to caking.

Solid forms of plant growth regulators offer a number of key ad-20 vantages, including convenience, increased stability and shelf life, as well as reduced packaging, storage and shipping costs.

Additionally, there is the possibility of future government regulation requiring solid forms of agricultural products in order to 25 reduce handling of contaminated packaging of these products during field application and during disposal. These dry flowable plant growth regulating compounds would be safer for the farmer to use and dispose of, and also result in a smaller volume of hazardous waste being produced.

There is a need for dry, flowable, highly concentrated powder and tablet formulations of hygroscopic plant growth regulators.

Surprisingly, free-flowing, non-caking solid mepiquat chloride 55 and chlormequat chloride formulations can be achieved by mixing the solid hygroscopic plant growth regulator with finely divided, highly absorptive inerts. In such mixtures, concentrations of the plant growth regulator of up to about 99 wt.-% are achievable. When the mixtures of the invention are directly applied in a 40 spray tank, the plant growth regulator dissolves instantly in the water without residues.

The preferred plant growth regulators of the present invention include the group consisting of 1,1-dimethyl-3,4-dehydro-45 piperidinium bromide, 4-chloro-1,1-dimethyl piperidinium bromide, 1,1-dimethylhexahydropyridazinium bromide, and 1,1-dimethyl-piperidinium chloride, also known as mepiquat chloride and

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2-chloroethyltrimethylammonium chloride, also known as chlormequat chloride.

It is an object of the present invention to provide an agricultu-5 rally acceptable hygroscopic plant growth regulator formulation in a solid form.

It is a further object of the present invention to provide methods of making the solid form of hygroscopic plant growth re-10 qulator compositions of the present invention.

It is another object of the present invention to provide an agriculturally acceptable hygroscopic plant growth regulator formulation in the form of a tablet.

It is a further object of the present invention to provide methods of making the dry, flowable tablet form of hygroscopic plant growth regulator compositions of the present invention.

20 These and other objects of the present invention will be more fully understood from the following description of the invention.

Figure 1 illustrates a spray dryer used in a method of the present invention.

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Figure 2 illustrates a double drum dryer used in a method of the present invention.

Figure 3 illustrates a batch vacuum dryer used in a method of the 30 present invention.

As used herein, the term "agriculturally acceptable" includes agricultural, industrial and residential use.

- 35 As used herein, "plant growth regulator(s)" (hereinafter abbreviated as "FGR") or "regulation" includes the following plant responses: inhibition of cell elongation, for example reduction in stem height and internodal distance, strengthening of the stem wall, thus increasing the resistance to lodding; compact growth.
- 40 in ornamentals for the sconomic production of improved quality plants; promotion of better fruiting; increasing the number of ovaries with a view to stepping up yield; promotion of senescence of the formation of tissue enabling fruit to absciss; defoliation of nursery and ornamental bushes and trees for mail-order busin-
- 45 ness in the fall; defoliation of trees to interrupt parasitic chains of infection; hastening of ripening, with a view to pro-

gramming the harvest by reducing the harvest to one to two pikkings and interrupting the food-chain for injurious insects.

As used herein, PGR formulations of the present invention may be 5 used to form both package and tank mix compositions.

The present preferred invention comprises PGR compositions comprising an agriculturally and plant growth regulating effective amount of a hygroscopic PGR, and more preferably, an N,N-dime-10 thylpiperidinium or N,N-dimethylammonium salt in a dry flowable highly concentrated powder.

Preferred PGRs include salts of the formula:

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where R is methyl or ethyl; X is the anion of an inorganic or organic, but not phytotoxic acid, preferably bromide or chloride, and the groups A independently denote methyl, ethyl or propyl which independently may be substituted by chloro or bromo, or the 25 groups A together denote a chain of 4 or 5 methylene groups, which chain may be substituted by chloro, bromo, methyl, chloromethyl, bromomethyl, hydroxymethyl, and methylene, or which chain containing one or two double bonds, or A is the chain -(C82)-MNE-, where n is 3 or 4, disclosed in U.S. Patent 3,905,798 and hereby 30 incorporated by reference.

Preferred specific examples of PGRS include 1,1-dimethyl-3,4-dehydro-piperidinium bromide, 4-chloro-1,1-dimethyl-piperidinium bromide, 1,1-dimethylhexahydropyridaxinium bromide, 1,1-dimethyl-35 piperidinium chloride and 2-chloroethyltrimethylammonium chloride.

The most preferred plant growth regulators are 1,1-dimethyl-piperidinium chloride, also known as N.N-dimethylpiperidinium chlo-do ride or mepiquat chloride, which is commercially available under the registered trademark Piv® (BASF AG, Germany) and 2-chloroethyltrimethylammonium chloride or chlormequat chloride, which is commercially available under the registered trademark Cycocel® (BASF AG, Germany).

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For convenience of description, mepiquat chloride will be used. However, the methods described apply equally to other hygroscopic PGRs, especially to chlormequat chloride.

5 In a preferred embodiment, silica is injected in the inlet air stream of a spray dryer at a controlled rate.

A spray dryer of the type illustrated in Figure 1 may be used. As can be shown from Figure 1, the aqueous PGR feed solution is agi10 tated in a feed tank (2) and fed through a line (4) via a feed
pump (6) into the spray dryer unit (8). The aqueous PGR feed solution is introduced into the spray dryer unit by an atomizing
means (10). An inlet air heating means (12) provides heat to the
dryer at a temperature of about 150 to about 250°C.

A flow aid such as silica is stored in a feed hopper (14) and injected into the spray dryer unit (8) via a screw feeder (16) through a line by an air eductor (18).

20 The silica adheres to the forming droplets or partially dried particles formed by the aqueous mepiquat chloride feed solution in the vicinity of the atomizer (10) and reduces or eliminates the tendency of the partially dried mepiquat chloride particles to stick to the spray drying unit walls (20, 22), the ducts (24), 25 and the cyclone (26). The silica also renders the powder more flowable, eliminating caking in the drum even when stored for long periods of time provided the drum excludes ambient moist air. The flowing powder is then suitable for commercial tabletting or for filling water soluble bags, e.g. made of polyvinyl 30 alcohol (EVA) films and marketed under trademarks as Monosol M70300 or Monosol M85320.

The rate at which the aqueous PGR feed solution is fed into the spray dryer unit is not critical and is dependent upon the size 35 of the spray dryer used. This rate is easily determined by those skilled in the art.

A preferred method dries the mepiquat chloride solution with a double drum dryer as illustrated in Figure 2. The double drum 40 dryer has a pair of hollow, rotating drums (28, 30) whose surfaces are scraped by a knife (32). Bigh pressures steam is introduced to the interior of the drums and mepiquat chloride solution added continuously via a feed line (34) to the nip between the drums (36). The drums turn toward one another, by means of a conveyor, for example 38 depositing a portion of the liquid, boiling mepiquat chloride solution on the drum surface (28, 30) where boiling is initiated. Upon further rotation, the thin film

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of mepiquat chlorida's water boils off into the vapor hood (40) and a solid film remains that is scraped by sharp knife (32) from the turning drum surface (28,30). The material is then collected and the flow aid is added to it to improve flowability and impart 5 anti-caking properties prior to tabletting or filling water soluble bags.

The plant growth regulator feed solution is preferably charged into the double drum dryer at a rate of about 5 gm/min. to about 10 200 gm/min. per square foot (about 9.3 dm²) of heated surface and the aqueous plant growth regulator is preferably charged into the double drum dryer into the nip between the drums.

A preferred embodiment of the drying process utilizes a batch va-15 cuum dryer with chopping blades which can also be described as a mechanical fluid bed. The most preferred batch vacuum dryer is a Littleford® type (or Lödige) vacuum dryer, as illustrated in Fidure 3.

- 20 As is seen from Figure 3, the vacuum dryer unit (52) consists of double jacket (42, 44). Inside the double jacket is a hollow rotating shaft (46) with attached plough shaped mixing elements (48).
- 25 Aqueous PGR feed solution is fed via a line (50) into the vacuum dryer unit (52). Steam or hot water (54) is fed via a line (56) into a jacket (42) which surrounds the vacuum dryer unit (52), and optionally through the hollow rotating shaft (45). Agitating means (57) in the interior of the vacuum dryer unit (52) agitates
- 30 the aqueous PGR feed solution. A vacuum means (58), which may be a pump or vacuum jet unit is introduced into and applied to the vacuum dryer unit (52). The vacuum and applied jacket heat causes the evaporation of the water from the aqueous PGR feed solution. The evaporated water boils up, passes through a bag collector.
- 35 means (60), and is recovered by a condenser (62) and collected in a condensate tank (64).

When a sufficient amount of water has been evaporated, a paste begins to form. Mixing elements (48) are used to divide the pa-40 ste, breaking it up, and bringing the interior moisture to the surface so as to expose it to the vacuum to increase the drying rate. As the material solidifies, the chopping means breaks the material into small particles to maintain the high drying rate.

45 A free-flowing, non-caking solid mepiquat chloride formulation can be achieved by mixing the solid mepiquat chloride with a finely divided, highly absorptive inert flow aid such as silica.

The addition of silica or other flow aid renders the powder flowable and non-caking, and suitable for tabletting or filling water soluble bags. The flow aid is introduced manually or mechanically through a port on or near the top of the drying chamber.

All three drying processes use silica or other flow aid to improve flowability and prevent caking. These inert additives include any form of silica including fumed silicas, precipitated silicas, aluminum silicates, magnesium silicates, and the like,

- 10 zeolites, bentoinites, montmorillonites, and attapulgites and mixtures thereof. The most preferred silica is commercially available as Sipernat® 50S, which is a synthetic amorphous silicon dioxide hydrate.
- 15 The weight of silica per weight of mepiquat chloride in all of these drying processes is about 0.2:100 to 3:100, and more particularly, about 2:100.

Optionally, to further improve flowability, reduce sticking ten-20 dency or caking, or to increase the dissolution rate, binders, fillers, and/or disintegrants can be dissolved in the feed solution before drving.

Suitable binders, fillers, and/or disintegrants include water-so-25 luble cellulose derivatives, cellulose derivatives, carboxymethyl cellulose, hydroxypropyl methylcellulose, water soluble gums such as gum arabic, gum tragacanth, alginates, gelatin, and polyvinylpyrollidone, cross-linked polyvinylpyrrolidone, microcrystalline cellulose, modified starches such as sodium carboxymethyl starch, 30 and mixtures thereof.

Preferred binders, fillers, and/or disintegrants are carboxymethyl cellulose.

- 35 Other suitable fillers, binders, and/or disintegrants include any water soluble starch, corn syrup, dextrin or pregelatinized starch which is at least partially soluble in water at ambient temperature. For example, there can be used as a binder the pregelatinized, modified and stabilized waxy maize starch which is
- 40 marketed by the National Starch and Chemical Corporation under the trade name Instant Celar Gel®. In addition, pregelatinized corn starch marketed by the Hubinger Company under the trade name OK Pre-Gel® can be used. Other binders suitable for use are pregelatinized food starch, refined from tapioca and marketed under
- 45 the trade name Instant Gel®; stable, modified amylopectin marketed under the trade name Kosol®; a low viscosity tapioca dextrin marketed under the trade name Crystal Gum®; dextrinized corn

starch marketed under the trade name Purity Glaze®; maltodextrin marketed under the trade name Maltrin®, such as M040 by Grain Processing corporation.

5 The preferred amount of binders, fillers, and/or disintegrants in the feed solution is from about 0.1 to about 99.7 wt.-*.

All of the above-described powders, with and without fillers, binders, and/or disintegrating agents can then be tabletted or 10 filled into water soluble bags. Unexpectedly, the high potency powders which contain only the hygroscopic PGR active material and silica flow aid, tablet without aid of binders, fillers, and/or disintegrants, or lubricants on a commercial tablet press. The tablets formed are of commercial quality, having reproducible 15 weight, sufficient tablet strength, and acceptable solublity.

Water absorbance is minimal provided that the tablets are made in a dehumidified room. The tablets can be dissolved and passed through a 50 mesh screen such as that found on spray equipment 20 without residue.

While the ratios of the concentrations of the various components of the present invention hereinafter suggested, those skilled in the art will recognize that minor variations may be necessary to 25 accommodate particular characteristics of acceptable plant growth regulators which may be employed in this invention.

In general, the formulations of the present invention contain from about 0.1 to about 99.8 wt.-%, and preferably from about 95 30 to about 99 wt.-% of active ingredient.

Typically, for a plant growth regulator concentrate of the present invention, the concentration of regulator active ingredient will be at least 6 ml/acre (about 0.0125 pints/acre).

In such mixtures, concentrations of mepiquat chloride up to about 99 wt.-% are achievable. When the mixtures of the invention are directly applied in a spray tank, the mepiquat chloride dissolves instantly in the water and this spray solution passes a 50 mesh 40 screen of the spray equipment without residues.

The tablets can be manufactured by compressing the mixtures on tablet machines. Also for tabletting, other inert ingredients like disintegrants, binders, fillers, and/or disintegrants, vertes ting agents or lubricants can be blended with the PGR mixture. (Optionally, the wetting agents and lubricants can be incorporated by addition in the drying step--either into the PGR liquid

solution before drying, or can be added with the inert flow aid during drying.)

When the tablets are dropped into the water of the spray tank, 5 the mepiquat chloride is quickly dissolved and this spray solution passes a 50 mesh screen of the spray equipment without residues.

In addition to the above-described components, the compositions 10 of the present invention may also include other ingredients or adjuvants commonly employed in the art.

Examples of such ingredients include drift control agents, defoaming agents, preservatives, surfactants, fertilizers, phytotoxi-15 cants, herbicides, pesticides, insecticides, fungicides, wetting agents, adherents, nematocides, bactericides, trace elements, synergists, antidotes, mixtures thereof and other such adjuvants well known in the plant growth regulator art.

20 However, it is preferred to employ the compositions of the present invention along with sequential treatments with these other components for optimal effect.

The compositions of the present invention may be applied to 25 plants. The application of liquid and particulate solid plant growth regulator compositions to above ground portions of plants may be carried out by conventional methods, for example, boom and hand application, including sprayers or dusters. The composition may be applied aerially as a spray, if desired. The mixtures of 30 the present invention are preferably used in the form of aqueous solutions. The mixtures are applied in a conventional manner, for example, by spraying, atomizing, watering or disinfecting seed.

The forms of application depend entirely on the purpose for which 3 the compositions are being used. In any event, they should ensure a fine distribution of the active ingredients in the composition.

The above plant growth regulator formulation may then be dispersed in water and sprayed onto plants according to the method of 40 the present invention.

Powders, dusts and broadcasting agents may be prepared by mixing or grinding the active ingredients with a solid carrier.

45 Granules, for example, coated, impregnated or homogeneous granules, may be prepared by bonding the active ingredients to solid carriers. Examples of solid carriers are mineral earths such as

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gilicic acid, silica gels, silicates, talc, kaolin, Attaclay, limestone, lime, chalk, bole, loess, clay, dolomite, diatomacecus earth, calcium sulfate, magnesium sulfate, magnesium oxide, ground plastics, fertilizers such as ammonium sulfate, ammonium 5 phosphate, ammonium mitrate, and ureas, and vegetable products such as grain flours, bark meal, wood meal, and nutshell meal, cellulosic powders, and the like

The action of the compositions of the present invention are opti10 mal even at low application rates. For a given plant growth regulator composition, the skilled artisan will readily arrive at a
composition having the optimum ratio of the ingredients by routime experimentation. The compositions of this invention may be
prepared, for example, by adding, in any order, the various com15 ponents of the composition of the present invention. For example,
one may start with a commercial formulation of mepiquat chloride,
which is an aqueous concentrate containing 42 gms/1 (about 0.35
pounds per gallon (US)) of mepiquat chloride (4.2 wt.-%). Thereafter, in any order, one mixes suitable amounts of any optional
20 adjuvants or ingredients.

The following examples serve to illustrate the invention and should in no way be construed as limiting the scope thereof.

25 Examples

Example 1 - Formulation

An aqueous solution of mepiquat chloride was dried to give a so-30 lid mepiquat chloride with a water content of 0.2 wt.-%. This product was not free flowing and caked in a sealed, tight container after 2 days of storage at room temperature. Directly after drying, 198 g solid mepiquat chloride were mixed with 2 g of Aerosi10 200 (highly dispersible, pyrogenic silicic acid, from 35 DEGUSSA, Germany) in a laboratory mixer to give a homogeneous mixture. After storage in a sealed container for 1 month at room temperature and 50°C, there was no caking.

The mixture remained free flowing. Twenty grams of the mixture 40 were poured into a laboratory spray tank filled with about 3.8 liters (1 gallon) tap water at room temperature. The mepiquat chloride dissolved completely within 1 minute. There was no residue on a 100 mesh screen of the laboratory spray tank.

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Example 2 - Water Soluble Bag

One hundred grams of the mixture described in Example 1 were pakkaged using a bag made of a water soluble polyvinyl alcohol film 5 (Monosol® M7030, from Chris-Craft Industries, USA). This water soluble bag was dropped into a spray tank filled with about 95 liters (25 gallons) tap water at room temperature. The water was circulated through a 50 mesh screen. The mepiquat chloride and the film of the bag dissolved completely within 10 minutes. There 10 was no residue on the 50 mesh screen.

Example 3 - Tablet Formulation

Minety-five gramms of the mixture described in Example 1 and 5 g 15 Divergan® F (finely powdered, crosslinked polyvinyl pyrrolidone, from BASF Corporation, USA) were blended in a laboratory mixer. A 15 g tablet, 5.7 cm (2 1/2 in.) diameter, was made with a hand operated hydraulic press. The tablet was dropped into a spray tank with tap water at room temperature. The tablet broke up com-20 pletely and the mepiquat chloride dissolved within 10 minutes. There was no residue on the 50 mesh screen of the spray tank.

Example 4 - Formulation

25 Directly after drying as described in Example 1, 294 g solid mepiquat chloride were mixed with 6 g Sipernat® 50 S in a laboratory mixer to give a homogeneous mixture. After storage in a sealed container for 1 month at room temperature and 50°C, there was no caking. The mixture remained free flowing.

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Twenty grams of the mixture were poured into a laboratory spray tank filled with about 3.8 liters (1 gal.) tap water at room temperature. The mepiquat chloride dissolved completely within 1 minute. There was no residue on the 100 mesh screen of the labostratory spray tank.

Example 5 - Water Soluble Bag

sidue on the 100 mesh screen.

One hundred grams of the mixture described in Example 4 were pak-40 kaged using a bag made of a water soluble polyvinyl alcohol film (Monosol 00 M8532, from Chris-Craft Industries, USA). This water soluble bag was dropped into a spray tank filled with about 95 liters (25 gallons) tap water at room temperature. The water was circulated through a 100 mesh screen. The mapiquat chloride and 45 the film dissolved completely within 10 minutes. These was no re12

Example 6 - Tablet Formulation

Using the mixture of Examples 4, 20 g tablets, 5.7 cm (2 1/2 in.) diameter, were made with a hand operated hydraulic press. Five 5 tablets were dropped into a spray tank filled with about 95 liters (25 gallons) tap water at room temperature. The tablets broke up completely and the mepiquat chloride dissolved within 12 minutes. There was no residue on the 100 mesh screen of the spray tank.

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Example 7 - Formulation

A 500 g/l solution of mepiquat chloride was placed in an agitated, jacketed, spray dryer feed tank and heated to 65°C with tem15 pered water. The heated solution was pumped at 125 g/min to an atomizing wheel rotating at about 17,000 rpm in a spray dryer (a Miro Utility for example). Silica (Sipernat® 505) from a loss-inweight screwfeeder was injected via an air eductor into the air plenum to mix with the heated air entering the plenum. The silica
20 was fed at a rate of 4 wt.-4 based on the dry basis feed rate of the mepiquat chloride solution. The silica/air mixture, at 200°C, then entered the drying chamber, intermixing with the droplets formed by the atomizer. The resultant outlet temperature is about 140°C. On drying the powder exits the drying chamber does not ad25 here to the walls of the spray dryer, the ducting, or the cyclone separator. The powder remains flowable in a polyethylene bag pakked in a sealed plastic drum.

The resulting powder was flowable, had a moisture content of 0.25 30 wt.-%, a bulk density of 0.29 g/ml untapped, 0.38 g/ml tapped, and an ash content of about 2 wt.-%. The powder assayed at about 97 wt.-% mepiquat chloride.

Example 8

Steam at 105 psig was introduced to a lab scale double drum dryer and the rolls rotated at about 5 rpm. Mepiquat chloride liquid was fed from a reservoir to the nip of the rolls at a rate of about 36 g/minute. The material adhered to the rolls and the moistore was evaporated while the drums rotated. The solid film was scraped off the rolls by a blade and collected. Material collected without silica rapidly caked. Material that was collected and mixed with about 2 wt.-% (Sipernat@ 505) silica did not cake and was flowable. The moisture content was about 1.2 wt.-% in the re-45 sultant powder, with a density of 0.25 g/ml untapped and 0.35 g/ml tanped.

Example 9

To a 130 liter Littleford "mechanical fluid bed" dryer (Model FKM-130 with chopping blade), about 78 kilograms (171.6 lbs) of 5 mepiquat chloride 600 g/l aqueous solution was charged. The agitator plough was started at 155 rpm, and 15 psig steam introduced to the jacket. A vacuum was pulled with a vacuum pump, maintaining 600 mm Hg at the pump. The evaporated vapors passed through a bag filter and were condensed using a cold glycol/water mixture 10 on the shell side of a condenser. The resulting condensate was collected in a receiver.

As evaporation continued, the amperage drawn by the plough motor began to rise. The chopper blades were turned on, and the drying 15 completed. During this time the steam pressure on the jacket was progressively increased to drive off the water from the forming paste. As more water was removed, the paste turned to solid, the chopper greatly increasing the rate of drying by dividing moist material and exposing the interior moisture to the vacuum and hot 20 dryer walls. When water was no longer being removed, the dried solid was cooled by applying cool water to the jacket of the apparatus. Approximately 2 wt.-% of silica was then added to the material and allowed to blend. When this mixing operation was complete, the finished product was discharged to a drum.

25 The resulting free flowing powder was composed of particles ranging from approximately 5 to 60 microns in diameter, with a moisture of about 0.08 wt.-%, and bulk density of 0.63 untapped and 0.79 tapped, and ash content of about 2 wt.-%. The powder assayed 30 at about 97 wt.-% mepiquat chloride. There was no detectable mepiquat chloride in the overhead condensate.

Example 10

35 About 4.5 kilograms (10 pounds) of powder made by the method in Example 9 was charged to the feed hopper of a single station excenter tablet press (Stokes R type for example) located in a low humidity room. The relative humidity of the room remained about 28% between about 21 and 27°C (70 and 80°F). The press was fitting 40 with tooling to make about 5.7 cm (2.25 inch) diameter tablets. After pressure and size adjustments, tablets were made of about 21 grams with good tablet integrity. Hardnesses, as measured on a RIMAC tester, were to about 9.5 kg (21 lbs) force. Tablets were found to have picked up less than 0.3 wt.-% moisture during this 45 operation.

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The tablets had thicknesses of about 0.8 to 0.9 centimeters. The tablets dissolved under mild agitation in water in about 7 to 9 minutes and the resulting liquid did not deposit any residue when passed through 150 micron sieve (100 mesh).

Whereas particular embodiments of the invention have been described above for purposes of illustration, it will be appreciated by those skilled in the art that numerous variations of the details may be made without departing from the invention as described in 10 the appended claims.

Example 11

A mepiquat chloride powder prepared by the method of (example 8
15 for drum dryer) was tabletted (by a Carver press for example).
Press pressure was varied at 6 to 7 metric tons, 8 to 9 metric
tons, and 10 to 11 metric tons for durations of 1 minute each.
The formed tablets, of 2.26 inches in diameter, had thicknesses
between 6.1 and 6.6 mm (0.24 and 0.26 inches) with weights of
20 between 15.3 to 15.6 gms, with breaking strengths between 4 and
10 kgs (9 and 22.3 lbs) as determined on a model ITC manual
test stand. The tablets were dissolved in 750 ml of 342 ppm hardness water stirred with a magnetic stirring bar and dissolved
25 completely in 0.9 to 4.7 minutes.

Example 12

A mepiquat chloride powder prepared by the method of (example 9 30 for the Littleford dryer) was tabletted (in a Carver press for example). Press pressure was varied at 8 to 9 metric tons, and 10 to 11 metric tons for durations of 1 minute each. The formed tablets, of 2.26 inches in diameter, had thicknesses between 6.1 and 6.6 mms (0.24 and 0.26 inches) with weights of between 15.3 to 15.7 gms, with breaking strengths between 7.7 and 14.5 kgs (17 and 32 lbs) as datermined on a modified Chatillon electronic tester, model DFI-50 mounted on a model LTC manual test stand. The tablets were dissolved in 750 ml of 342 ppm hardness water stirred with a magnetic stirring bar and dissolved completely in 4.4 40 to 5.8 minutes.

Example 13

A mepiquat chloride powder prepared by the method of (example 7 45 for the spray dryer) was tabletted (in a Carver press for example). Press pressure was varied at 6 to 7 metric tons, 8 to 9 metric tons, and 10 to 11 metric tons for durations of 1 minute

each. The formed tablets, of 5.74 cms (2.26 inches) in diameter, had thicknesses between 5.8 and 7.1 mms (0.23 and 0.28 inches) with weights of between 14.4 to 15.7 gms, with breaking strengths between 7.48 and 24.9 kgs (16.5 and 55 lbs) as determined on a 5 modified Chatillon electronic tester, model DFI-50 mounted on a model LTC manual test stand. The tablets were dissolved in 750 ml

model LTC manual test stand. The tablets were dissolved in 750 of 342 ppm hardness water stirred with a magnetic stirring bar and dissolved completely in 3.8 to 4.8 minutes.

10 Whereas particular embodiments of the invention have been described above for purposes of illustration, it will be appreciated by those skilled in the art that numerous variations of the details

may be made without departing from the invention as described in the appended claims.

Claims

What is claimed is:

- A plant growth regulator formulation in solid form comprising an effective amount of a hygroscopic plant growth regulator.
- The formulation of claim 1 wherein said plant growth regulator is mepiquat chloride or chlormequat chloride.
- A method of making a dry, flowable powder of an aqueous hygroscopic plant growth regulator using a spray dryer comprising: drying said hygroscopic plant growth regulator and miting an effective amount of an inert.
- 4. A method of making, a dry, flowable powder of a hygroscopic plant growth regulator using a spray dryer comprising; injecting aqueous plant growth regulator feed solution into said of spray dryer at a controlled rate; and injecting an inert in the inlet air stream of said spray dryer at a controlled rate; whereby the inert adheres to droplets of said plant growth regulator forming a dry, flowable powder.
- 25 5. A method of making a dry, flowable powder of a hygroscopic plant growth regulator using a double drum dryer comprising: charging aqueous plant growth regulator feed solution into said double drum dryer with interior pressurizing means and scraping means, at a continuous rate; rotating each drum of said double drum dryer toward the other which deposits a portion of the aqueous plant growth regulator feed solution on the interior drum surface, and forms a solid film of plant growth regulator; removing said solid film by scraping means to form a dry, flowable powder.
- A method of making a dry, flowable powder of a hygroscopic plant growth regulator using a batch vacuum dryer comprising: charging aqueous plant growth regulator feed solution into said batch vacuum dryer with chopping means, agritation means and steam jacket, at a controlled rate; applying steam to said jacket; applying a vacuum to said batch vacuum dryer by a vacuum means; agritating said feed solution in said batch vacuum dryer; evaporating the water from said aqueous plant growth regulator feed solution thereby forming a paste; and thopping said paste to form a dry, flowable powder.

7. A powder formed by one of the methods of claims 3 to 6.

8. A tablet formed from the powder of claim 7.

5 9. A water soluble bag comprising the powder of claim 7.

High Concentrated, Solid Mepiquat Chloride and Chlormequat Chloride Products

5 Abstract of the Disclosure

The present invention provides hygroscopic plant growth regulator formulations in solid forms and associated methods of making the prowders and tablets. The most preferred formulation uses an 10 effective amount of an N,N-dimethyl-piperidinium and/or N,N-dimethylammonium salt.

AMENDED CLAIMS

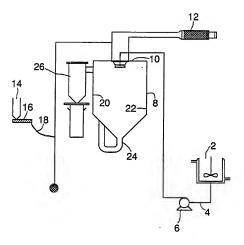
[received by the International Bureau on 09 December 1994 (09.12.94); original claims 1,2,3-6 amended; remaining claims unchanged; claims renumbered 1-8 (2 pages)]

- A plant growth regulator formulation in solid form comprising a synthetic amorphous silicon dioxide hydrate and an effective amount of 1.1-dimethylotperidinium chloride.
- A method of making a plant growth regulator formulation as claimed in claim 1, using a spray drier comprising:
 - (i) drying 1,1-dimethylpiperidinium chloride and .
 - (ii) mixing an effective amount of a silica.
- A method of making a plant growth regulator formulation as claimed in claim 1, using a spray drier comprising:
 - injecting an aqueous feed solution of 1,1-dimethylpiperidinium chloride into said spray drier at a controlled rate; and
 - (ii) injecting a silica into the inlet air stream of said spray drier at a controlled rate.
- 4. A method of making a plant growth regulator formulation as claimed in claim 1, using a double drum drier comprising:
 - charging an aqueous feed solution of 1,1-dimethylpiperidinium chloride into said double drum drier with interior pressurizing means and scraping means, at a continuous rate;
 - (ii) rotating each drum of said double drum drier toward the other;
 - (iii) removing the solid film formed on the interior drum surface by scraping means.

- A method of making a plant growth regulator formulation as claimed in claim 1, using a batch vacuum drier comprising:
 - charging aqueous feed solution of 1,1-dimethylpiperidinium chloride into said batch vacuum drier with chopping means, agitation means and steam jacket, at a controlled rate;
 - (ii) applying steam to said jacket;
 - (iii) applying a vacuum to said batch vacuum drier by a vacuum means;
 - (iv) agitating said aqueous feed solution in said batch vacuum drier;
 - (v) evaporating the water from said aqueous feed solution;
 - (vi) pulverizing the paste formed in step (v) by chopping.
- 6. A powder formed by one of the methods of claims 2 to 5.
- A tablet formed from the powder of claim 6.
- 8. A water soluble bag comprising the powder of claim 6.

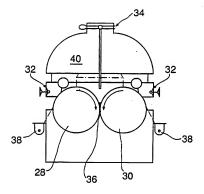
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FIG.1



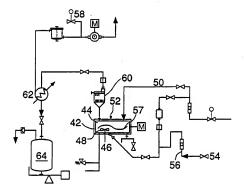
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FIG.2



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FIG.3



INTERNATIONAL SEARCH REPORT Inte. onal Application No

| | | PC* | T/EP 94/02253 |
|-----------------------|---|--|---|
| ÎPC 6 | SIFICATION OF SUBJECT MATTER A01N43/40 A01N33/12 A01N25 | /12 | |
| According | to International Patent Classification (IPC) or to both national cla | mification and IPC | |
| | S SEARCHED | | |
| IPC 6 | iorumentation searched (classification system followed by classific AOIN | etion symbols) | |
| Documenta | tion scarched other than minimum documentation to the extent thi | st such documents are moluded in | the fields searched |
| Electronic o | late bass consisted during the international search (name of data b | are and, where practical, search | ternos used) |
| C. DOCUM | SENTS CONSIDERED TO BE RELEVANT | | |
| Category * | Citation of document, with indication, where appropriate, of the | relevant passages | Relevant to claim No. |
| X | DD,A,101 386 (E. FIBITZ ET AL.) 1973 see page 2 - page 3 | 5 November | 1-9 |
| X,P | EP,A,O 573 177 (MICRO-FLO) 8 Dec 1993 | ember | 1,2,7-9 |
| X,P | WO,A,94 09627 (BASF) 11 May 1994 see page 1, line 19 - page 2, li | ne 20 | 1,2 |
| X | FR,A,2 172 418 (BASF) 28 Septemb see page 3, line 36 see page 5, line 34 - line 36 | er 1973 | 1,2,7,8 |
| ^ | US,A,3 356 569 (D.O. NICODEMUS E December 1967 see column 1, line 37 - column 2 | • | 4 |
| | | -/ | |
| | er documents are listed in the continuation of box C. | Patent family members | are listed in annex. |
| | ogorses of cited documents : ont defining the general state of the art which is not ared to be of particular relevance | "T" later document published at or priority date and not in cited to understand the pris | her the international filing date conflict with the application but sciple or theory underlying the |
| 'E' cartier of | locument but published on or after the international | "X" document of particular rele cannot be considered novel involve an inventive step w | hen the document is taken alone |
| *O* docume other n | or other special reason (as specified) nt referring to an oral disclosure, use, exhibition or seans | document is combined with | vance; the claimed invention rolve an inventive step when the cone or more other such docu- ting obvious to a person skilled |
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| | ctual completion of the international rearch | Date of mailing of the intern | national search report |
| | October 1994 | 0 7. 11. 94 | |
| rvame and m | ailing address of the ISA European Patent Office, P.B. 5818 Patentiann 2 NL - 2280 HV Rijewijk Tel. (+ 31-70) 340-2340, Tx. 31 651 epo nl, | Authorized officer | |
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- 1

INTERNATIONAL SEARCH REPORT

Inte mal Application No PCT/EP 94/02253

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT Category * Citation of document, with indication, where appropriate, of the relevant passages Relevant to claim No. EP,A,O 518 629 (RHONE-POULENC AGROCHEMIE) 16 December 1992 see page 1, line 24 - line 27 see page 4, line 32 - line 33 9

1

INTERNATIONAL SEARCH REPORT

Information on patent family members

Inter mai Application No PCT/EP 94/02253

| Publication data 08-12-93 11-05-94 28-09-73 | NONE NONE AU-B- DE-A- AT-B- BE-A- | 5150893 2207575 | Publication date 24-05-94 23-08-73 |
|--|---|---|--|
| 11-05-94 | NONE AU-B- DE-A- AT-B- BE-A- | 2207575 | |
| 11-05-94 | AU-B- DE-A- AT-B- BE-A- | 2207575 | |
| | DE-A- AT-B- BE-A- | 2207575 | |
| 28-09-73 | AT-B- BE-A- | | 23-08-73 |
| | CH-A- GB-A- JP-C- | 321026 795534 567353 1414259 1157912 | 10-03-75 16-08-73 15-10-75 19-11-75 25-07-83 |
| | JP-A- JP-B- NL-A- SE-B- US-A- | 48088230 57045203 7301819 382154 3905798 | 19-11-73 27-09-82 21-08-73 19-01-76 16-09-75 |
| | BE-A- FR-A- GB-A- | 663212 1508063 1095985 6505570 | 29-10-65 |
| 16-12-92 | US-A- AU-A- AU-A- CA-A- CA-A- CN-A- CN-A- EP-A- JP-A- JP-A- JP-A- NZ-A- NZ-A- | 5139152 1802392 1809192 1809192 2071075 2071076 2071077 1067859 1067629 0524721 0522713 5155704 5155708 243095 243096 | 18-08-92 24-12-92 17-12-92 17-12-92 12-12-92 12-12-92 12-12-92 13-01-93 06-01-93 06-01-93 27-01-93 13-01-93 22-06-93 22-06-93 22-06-93 22-09-94 27-09-94 |
| | | | |
| | 16-12-92 | SE-B- US-A- FR-A- GB-A- NL-A- 16-12-92 US-A- AU-A- AU-A- AU-A- CA-A- CA-A- CA-A- CH-A- CH-A- CH-A- CH-A- CH-A- CH-A- DP-A- JP- | SE-B- 382154 US-A- 3905798 BE-A- 65212 FR-A- 1508063 GB-A- 1095985 NL-A- 6505570 16-12-92 US-A- 5139152 AU-A- 1802392 AU-A- 1802392 AU-A- 1809192 CA-A- 2071076 CA-A- 2071076 CA-A- 1067639 CN-A- 1067639 CN-A- 1067639 EP-A- 0524721 SP-A- 5155704 JP-A- 5155704 JP-A- 5155704 JP-A- 5155704 JP-A- 243095 |

INTERNATIONAL SEARCH REPORT

information on patent family members

tnter. nal Application No PCT/EP 94/02253